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Characterizations of partially reduced polyoxometalate catalysts using ammonia adsorption microcalorimetry and methanol oxidation studies / by Suresh Babu Bommineni.

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**CHARACTERIZATIONS OF PARTIALLY REDUCED
POLYOXOMETALATE CATALYSTS USING AMMONIA
ADSORPTION MICROCALORIMETRY AND METHANOL
OXIDATION STUDIES**

By

Suresh Babu Bommineni

A THESIS

Submitted in partial fulfillment of the requirements for the degree of

MASTER OF SCIENCE

(CHEMICAL ENGINEERING)

MICHIGAN TECHNOLOGICAL UNIVERSITY

2011

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This thesis, "Characterizations of Partially Reduced Polyoxometalate Catalysts Using Ammonia Adsorption Microcalorimetry and Methanol Oxidation Studies," is hereby approved in partial fulfillment of the requirements for the Degree of MASTER OF SCIENCE IN CHEMICAL ENGINEERING.

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Abstract

Phosphomolybdic acid ($\text{H}_3\text{PMO}_{12}\text{O}_{40}$) along with niobium, pyridine and niobium exchanged phosphomolybdic acid catalysts were prepared. Ammonia adsorption microcalorimetry and methanol oxidation studies were carried out to investigate the acid sites strength acid/base/redox properties of each catalyst. The addition of niobium, pyridine or both increased the ammonia heat of adsorption and the total uptake. The catalyst with both niobium and pyridine demonstrated the largest number of strong sites. For the parent $\text{H}_3\text{PMO}_{12}\text{O}_{40}$ catalyst, methanol oxidation favors the redox product. Incorporation of niobium results in similar selectivity to redox products but also results in no catalyst deactivation. Incorporation of pyridine instead changes to the selectivity to favor the acidic product. Finally, the inclusion of both niobium and pyridine results in strong selectivity to the acidic product while also showing no catalyst deactivation. Thus the presence of pyridine appears to enhance the acid property of the catalyst while niobium appears to stabilize the active site.

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Chapter 1

Introduction

In modern chemical industries today, more than 60% of the chemicals and intermediates synthesized via catalytic processes are done by oxidation [1, 2]. Oxidation reactions play an important role in the total catalytic oxidation where the desired products are obtained and also the destruction of undesired products [3]. In catalytic selective oxidation reactions the surface acidity/basicity and redox properties of the metal oxides play an important role.

Selective oxidation is extensively carried out on light hydrocarbons or alkanes like ethane, propane and butane[4], to obtain products such as acetic acid, acrylic acid and maleic acid. The work is focusing on ethane and propane because they are readily available and cheap[1]. Production of acetic acid and acrylic acid from ethane and propane are not commercial today. Production of maleic acid from butane is commercial in industry today. One of the well known selective oxidation reaction that is commercial in industry today is the conversion of n-butane to maleic anhydride over vanadium phosphorous oxide catalyst [1, 2].

In the chemical industries, the selective oxidations of hydrocarbon reactions continue to play an important role, resulting in ongoing investigation of the heterogeneous catalysts that accomplish these reactions. Polyoxometalates and phosphomolybdates have been extensively investigated for the selective oxidation of light alkanes [5-7]. The reason that these heterogeneous catalysts and their salts are usually investigated for their ability to

perform selective oxidation reactions is because their structure and composition can be finely controlled. One of the major challenges is to determine the surface active sites on the metal oxides to understand the fundamental catalytic relationships for metal oxide catalysts [8]. The nature of active sites, their number and their strength on the catalyst surface, determines the selectivity and conversion capabilities of the catalyst. The nature of the oxide, the charge and the radius of the metal ions, will have an effect on the acidity and basicity of the catalyst [9].

1.1 Catalyst

The commercial use of heteropolyacid catalysts (HPA's) in some process have already been carried out. One of the main advantages is the reduced need for separation of solid heteropolyacids over liquid acids.[10-13] . The HPA's consists of primary, secondary and tertiary structures. Keggin – type HPA's are the most commonly known primary structure and are also thermally stable [14]. A simple Keggin unit is shown in figure (1-1). The general formula for the keggin-type HPA is $QM_{12}O_{40}^{x-}$, where Q is the central atom consisting of either P, Si or Ge and M being the transition-metal atom commonly consisting of either molybdenum or tungsten and x being the charge on the structure. The central atom of a primary structure consists of tetrahedral arrangement of oxygen atoms which is surrounded by 12 oxygen octahedra-transition-metal. A keggin unit consists of four types of oxygen atoms, one central oxygen atom, one terminal oxygen atom and two different types of bridging atoms [10, 15]. The bridging atoms form single bonds to the two different transition-metal atoms, and the double bond to a single transition-metal atom is formed by the terminal oxygen atom[13].When the keggin unit is located at the

lattice position, the secondary structure takes the form of Bravais lattices. The number of waters of hydration found in the solid will determine if it is a secondary structure[12]. Water bridges are formed in the secondary structure when the water of crystallization in the HPA's binds the keggin units.[13] . When heavy alkali salts are present or produced, tertiary structures are formed[13].

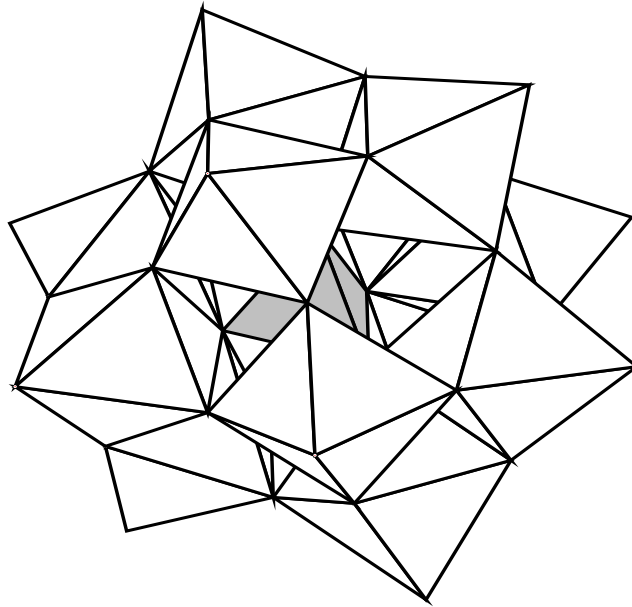


Figure (1-1): Keggin unit $\text{PMo}_{12}\text{O}_{40}^{3-}$ [1]

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In this work, the catalysts that are investigated include:

- 1) $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ [Phosphomolybdic acid hydrate]
- 2) $\text{NbPMo}_{12}\text{O}_{40}$ [Niobium exchanged phosphomolybdic acid]
- 3) $\text{PMo}_{12}\text{O}_{40}\text{pyr}$ [Pyridine exchanged phosphomolybdic acid]
- 4) $\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$ [Niobium and pyridine exchanged phosphomolybdic acid]

Previously the above catalysts were studied by Holles et al., for the selective oxidation of n-butane. In the previous work, it was found that the catalyst with the combination of niobium and pyridine was the most active and had high selectivity [1]. These studies were done to see how the selectivity and reactivity of the catalysts changed with the addition of niobium and pyridine. Li and Ueda showed that treating $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ catalyst with pyridine and then activating in nitrogen at 420°C improved the activity for the selective oxidation of propane to acrylic acid [16].

1.2 Microcalorimetry

The surface acid and base sites distributions on oxide surfaces can be determined through microcalorimetric studies [17-20]. Microcalorimetry studies help in determining the strength of the acidic sites exposed on the solid surface of the catalyst. The distribution of these sites is necessary to understand the catalytic properties. The conversion and selectivity of a reaction are influenced by the nature of the active sites, their number and also their strength. Auroux and Gervasini have reported the study of acidity and basicity on metal oxides surfaces[9] and have used microcalorimetry in order to determine the

number and character of basic and acidic surface sites. Several other papers have also studied the acidity of heteropolycomponents using ammonia absorption[10, 15, 21, 22].

Previously, methods such as titration with Hammett indicators, temperature-programmed desorption, adsorption microcalorimetry, catalytic probe reactions and NMR spectroscopy were used to determine the solid acids for the strength and number of sites[23]. Interactions with acid sites in solids are usually studied with ammonia because it is one of the simplest molecules and is also the most studied basic probe molecule[15]. Strong acids bind more strongly with ammonia than weaker acids. The choice of the base probe molecule is important in order to aptly characterize the surface. Ammonia is used because it is a small molecule and has affinity to base catalysts and most of the acid sites can be detected by ammonia [9, 10].

The calorimetric determination of heats of adsorption of bases produces curves of the type of differential heat of adsorption as a function of amount adsorbed, from which the distribution of adsorption sites over adsorption energies can be obtained[24]. This information gives details of the concentration of acid sites with different strengths in catalysts and also for identifying the relation between acidity and activity of different catalytic reactions[24]. In this study, chemisorption is of interest and is an essential step in heterogeneous catalysis, therefore, the bonding strength between the adsorbate and surface is an important parameter[25]. The activation energy of the surface reaction and also the surface concentration of the reactants can be affected depending on the strength of the chemisorptions bond[25]. Therefore the determination of the heats of adsorption of

gas-phase molecules on strong active sites is of importance and it should also be noted that the values of heat of adsorption can indicate not only the strength of the interaction on the surface of the catalyst but also the properties on it [25].

Previously, Bardin et al have reported the heat of ammonia adsorption for $H_3PMO_{12}O_{40}$ catalyst to be around 100 KJ/mol at 573 K and 120 KJ/mol at 473 K. They had very few sites at 573K and ammonia uptake of about 200 ($\mu\text{mol/g}$). But when the temperature was decreased to 473K, they ended up having more number of sites and higher ammonia uptake of above 1000 ($\mu\text{mol/g}$). This shows that the strength of the sites was high at 473K[10]. Jozefowicz et al have shown that $H_3PMO_{12}O_{40}$ activated at 423K had initial heat of adsorption of about 200 KJ/mol and at 523K the heat of adsorption dropped to 150 KJ/mol[26]. Lapkin et al have also shown similar result for the heat of adsorption for $H_3PMO_{12}O_{40}$ [27]. It can be noted that as pretreatment temperature increases, the initial heat of adsorption decreases. The strength of the sites also decreases with increase in temperature.

Jin et al have shown that the heat of adsorption of Nb_2O_5 at 373K was 80 KJ/mol[28]. But, recently Sun et al have reported that the ammonia adsorption at 423K for Nb_2O_5 had an initial heat of adsorption of 150 KJ/mol with an ammonia uptake of about 280 ($\mu\text{mol/g}$)[29]. Interestingly, Petre et al did not find any change in the heat of adsorption for Nb_2O_5 at 353K and 423K; at both the temperatures it was at 125KJ/mol[30]. Xue et al have reported the heat of adsorption of MoO_3 to be as low as 20KJ/mol with an ammonia uptake of 125 ($\mu\text{mol/g}$)[31]. Bardin et al have performed acidity of keggin type

heteropolycompounds by a number of methods including ammonia adsorption microcalorimetry[10, 15] . Xie et al shows the use of microcalorimetry to investigate the acid site distribution on carbons[21].

1.3 Methanol Oxidation

Work of Holles et al, Ueda and Suzuki showed that a molybdovanadophosphoric acid (PMo_{11}V) when treated with pyridine results in an active and selective catalyst for the conversion for propane to acrylic acid[1, 32]. Later, Li and Ueda showed that when pyridine is added to molybdophosphoric acid ($\text{H}_3\text{PMo}_{12}$) and heated to 420°C to activate the catalyst in presence of nitrogen, it improved the activity for the selective oxidation of propane to acrylic acid[1, 16]. By preheating the catalyst sample to 420°C all the organic components from the catalysts precursors are removed [14]. It also helps in finding out if the catalyst holds on to its properties at high temperature or if there is any change in it.

Methanol oxidation has been recognized as a dependable chemical probe of metal oxide catalysts through comparison of the catalytic activity and product selectivity[33]. To study the surface metal oxide redox sites, the reactivity of oxidative catalysts can be done by methanol oxidation reaction [34-38]. Methanol oxidation as discussed in the review of Tatibouët [33] refers to the network of oxidation and dehydration reactions. The reason for choosing methanol as the probe molecule to determine the number of surface active sites on pure metal oxides is due to the commonality of the surface methoxy intermediate formed during dissociative chemisorptions of methanol and methanol oxidation on the oxide catalysts [8]. In addition, methanol has high reactivity towards metal oxides [8].

Methanol oxidation reactions on metal oxide surfaces are very sensitive to the nature of active catalytic sites[33]. Methanol molecules are initially adsorbed on the surface metal sites as methoxy (CH_3O) species during the partial oxidation of methanol [34-39]. The products formed after the methanol oxidation reactions are formaldehyde, methylformate, dimethoxymethane, dimethyl ether and carbon oxides. The product distribution is determined by the nature of the surface active sites [3].The dehydration product yields the acid sites, that is dimethyl ether. The carbon oxides in the catalyst yield basic sites. The redox sites yield formaldehyde, methylformate and dimethoxymethane.

The knowledge of the number of surface active sites enables the calculation of the catalytic activity during methanol oxidation. The acid, base and redox properties of the products formed after methanol oxidation reaction can be analyzed for a range of pure metal oxides catalysts. These findings will help in better understanding of the catalysts and hopefully provide new insight into the fundamental catalytic properties of pure metal oxides.

Previous methanol oxidation studies have been carried out on molybdenum oxide catalysts, niobium oxide catalysts, vanadium oxide catalysts and other oxides by Wachs et al [3, 34, 40]. They have shown that MoO_3 had more selectivity for redox than acid product, Nb_2O_5 had only acidic product selectivity and V_2O_5 had very high selectivity for redox product compared with that of acidic product[3, 34, 40].

1.4 Aims/Goals of thesis:

The aim of this study is to show how the two distinct aspects of selective oxidation, acid/base strength and redox properties, contribute to the high activity of the heteropolyacids when niobium and pyridine are added on to them. Also to better understand the acid, base and redox properties of the catalysts. The catalyst we used are phosphomolybdic acid ($\text{H}_3\text{PMo}_{12}\text{O}_{40}$), pyridine exchanged phosphomolybdic acid ($\text{PMo}_{12}\text{O}_{40}\text{pyr}$), niobium exchanged phosphomolybdic acid ($\text{NbPMo}_{12}\text{O}_{40}$) and niobium and pyridine exchanged phosphomolybdic acid ($\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$) catalysts. Here the methods used to study the properties of these catalysts are ammonia adsorption microcalorimetry (acid/base aspect) and methanol oxidation reaction (redox aspect).

In the present work, we report how the introductions of niobium and pyridine on the parent catalyst, $\text{H}_3\text{PMo}_{12}\text{O}_{40}$, have an effect in the heat of adsorption of the catalysts by ammonia adsorption microcalorimetry. We further discuss about the nature of active sites present on the catalyst surface through product distribution. This is done by methanol oxidation reaction, which gives information about the acid, base and redox sites of the catalyst surface. The effect of metal oxides on the selectivity and strength of the catalyst can be found. This helps in better understanding of the polyoxometalate catalysts. The activity of the catalysts is also discussed during methanol oxidation.

The results obtained from our study are compared to the results obtained from other literature, carried out using the same methods to study the properties of other similar catalysts. Some authors have used the same catalysts but different probe molecule and

other authors have used the metal oxides in their study. Nevertheless, comparing the data with other literature helps in identifying efficient catalysts for industrial use and also to better understand the fundamental properties of the catalysts.

Chapter 2

Catalyst Preparations

1) $\text{H}_3\text{PMo}_{12}\text{O}_{40}$

Phosphomolybdic acid hydrate ($\text{H}_3\text{PMo}_{12}\text{O}_{40}$) was purchased from Aldrich and used directly.

2) $\text{NbPMo}_{12}\text{O}_{40}$

Niobium exchanged phosphomolybdic acid ($\text{NbPMo}_{12}\text{O}_{40}$) catalyst was prepared by using a known method from literature [1]. Niobium pentachloride (NbCl_5) was purchased from Aldrich. The solution of Niobium pentachloride (0.3025g) and water (2.5mL) was basified with ammonium hydroxide (0.125 mL). The white precipitate formed was then removed by filtration and the product was dissolved in an aqueous oxalic acid (0.252g in 5 mL water) to form niobium oxalate solution. The niobium oxalate solution was then added slowly to $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ (5g) dissolved in water (10 mL). The liquid was then evaporated completely by heating and stirring the mixture continuously.

3) $\text{PMo}_{12}\text{O}_{40}\text{pyr}$

Pyridine exchanged phosphomolybdic acid ($\text{PMo}_{12}\text{O}_{40}\text{pyr}$) catalyst was prepared by first dissolving phosphomolybdic acid hydrate ($\text{H}_3\text{PMo}_{12}\text{O}_{40}$) (3g) in water and then adding an aqueous solution of pyridine (0.4205 mL in 2.5 mL water) to the solution. The liquid was then evaporated completely by heating and stirring the mixture continuously[1].

4) NbPMo₁₂O₄₀pyr

Similar procedure was used to prepare niobium and pyridine exchanged phosphomolybdic acid (NbPMo₁₂O₄₀pyr) catalyst. Niobium exchanged phosphomolybdic acid (NbPMo₁₂O₄₀) catalyst was prepared by the method shown above. The obtained niobium exchanged phosphomolybdic acid (NbPMo₁₂O₄₀) (2g) was dissolved in water. To this solution an aqueous solution of pyridine (0.252 mL in 2.5ml water) was added. The liquid was then evaporated by heating and stirring the mixture continuously.[1]

2.1 Experimental Setup

The equipments used for the experiment consisted of gas and liquid units such as gas cylinders, mass flow controllers, methanol bubbler, reactor and GC/MS as shown in figure (2-1). The reactor setup consisted of a methanol bubbler, digital flow rate controller (Omega), a packed bed reactor and a GCMS (Finnegan, Trace GC ultra, Trace DSQ, Thermo Electron Corporation). The digital flow rate controller was used to control the flowrate of helium and oxygen gaseous mixture that is flowed through the methanol bubbler. The catalysts were placed in a glass tube of 6 mm and were supported by glass wool. The reactor was a downflow reactor operating at atmospheric pressure. The reactant flow was a single pass. Each catalyst sample run was pretreated to 420°C for 6 hours and held at the same temperature for 4 hours and then cooled to 260°C in 1 hour in presence of helium flow. Feed gases consisted of helium compressed (UN 1046, 5.0 ultra high purity, (UHP)) and oxygen compressed (UN 1072). The effluent from the reactor was connected to the GC/MS where the analysis was done.

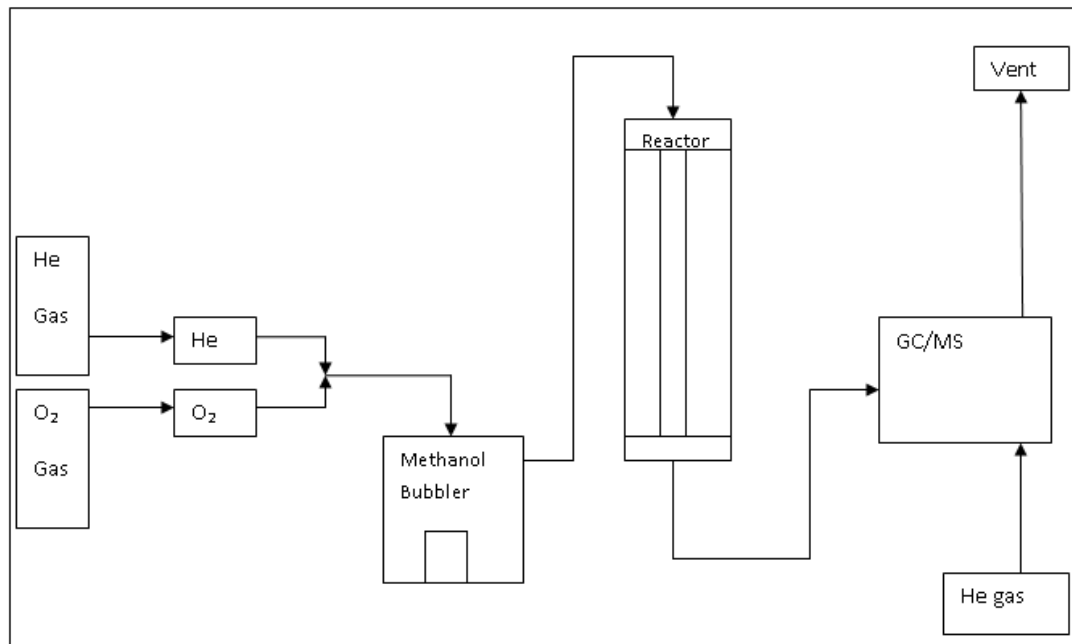


Figure (2-1): Experimental Setup

2.2 Mass flow controller calibration:

Digital flow rate controllers (Omega, model-FMA 78P4) were used to control the gas flow rates to the methanol bubbler. The flow controllers were calibrated using a glass bubble flow meter operating at room temperature and atmospheric pressure. The calibration results are plotted in figures (2-2) and (2-3) for helium and oxygen mass flow controllers respectively. These controllers enabled precise control of reactant concentrations and flow rates. To maintain low conversion, about ~10%, flow rates were changed for each catalyst during methanol oxidation.

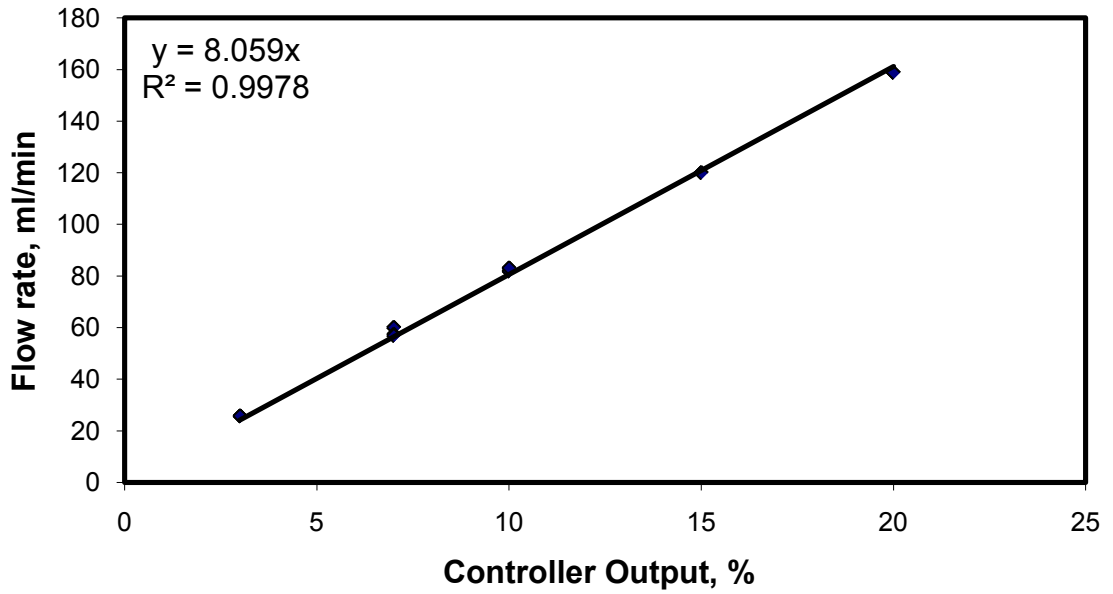


Figure (2-2): Helium Mass Flow Controller Calibration Results

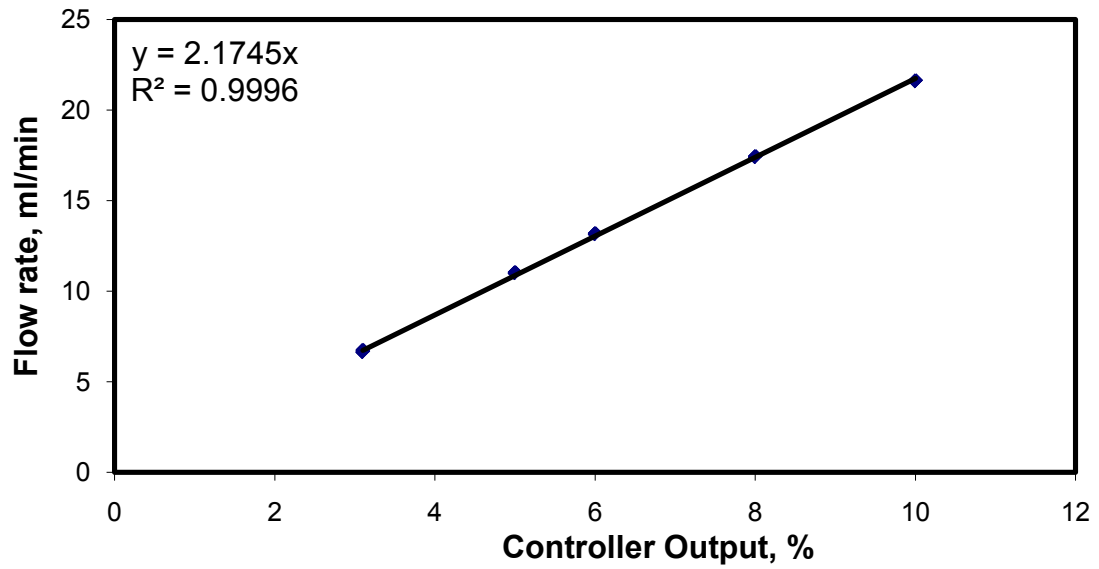


Figure (2-3): Oxygen Mass Flow Controller Calibration Results

2.3 GC/MS description and Setup

The GC/MS used was Finnegan, Trace GC ultra, Trace DSQ, Thermo Electron Corporation. The column used in the GC/MS was EquityTM-1, fused silica capillary column (30m*0.25mm*0.25µm film thickness). The column temperature was maintained at 50°C throughout the entire analysis.

2.4 Run procedure: Methanol Oxidation

The reactivity of supported phosphomolybdic acid derived catalysts was probed by the methanol oxidation reaction. The reactor setup consisted of a methanol bubbler, digital flow rate controller (Omega), a packed bed reactor and a GCMS (Finnegan, Trace GC ultra, Trace DSQ, Thermo Electron Corporation). The digital flow rate controller was used to control the flow rate of helium and oxygen gaseous mixture that is flowed through the methanol bubbler. The catalysts were placed in a glass tube of 6 mm and were supported by glass wool. The reactor was a downflow reactor operating at atmospheric pressure. The reactant flow was a single pass. Each catalyst sample run was pretreated to 420°C for 6 hours and held at the same temperature for 4 hours and then cooled to 260°C in 1 hour in presence of helium flow. This treatment is consistent with pretreatment procedures of this catalyst from the literature [17].

The methanol bubbler was connected to the reactor and the outlet from the reactor was connected to the GC. The outlet connected to the GC was heated to 100°C, so that any condensation of the products in the line can be avoided and also to remove traces of water formed during the reaction. Feed gases consisted of helium compressed (UN 1046, 5.0

ultra-high purity, (UHP)) and oxygen compressed (UN 1072). Initially oxygen and helium with the required flowrate is bubbled through methanol in the bubbler and run without the catalyst in the glass tube, so as to obtain the methanol count. Molar feed ratio into the GCMS taken was mixture of He/O₂/MeOH at the ratio 5.6:1:1.3, the reaction was run at a standard temperature of 260°C for all the catalysts, the flowrates of helium and oxygen modified as required and the catalyst weight (0.01gm to 0.04gm) was taken to obtain around 10% methanol conversion. Once feed was initiated to the reactor, the catalytic runs were taken for 2-3 hours with samples at an interval of 4 min, beginning 10 min after the methanol flow to the reactor was initiated. Product analysis was done by using the GCMS (Finnegan, Trace GC ultra, Trace DSQ, Thermo Electron Corporation) with a Equity™ -1, fused silica capillary column(30m*0.25mm*0.25µm film thickness). The selectivity of the products is defined in mole percentages.

2.5 GCMS Calibration:

Calibration of the GC/MS was done for the feed methanol and all the products of interest. The main by-products of the catalysts under study from methanol oxidation were dimethoxymethane, dimethyl ether and formaldehyde. From these calibrations the GC/MS counts can be converted to moles of each product. Determination of the number of moles of each product formed allows calculation of reaction rate and selectivity. The calibration of the GC/MS for methanol feed and each product is shown in the figures (2-4), (2-5), (2-6) and (2-7).

Methanol, formaldehyde and dimethoxymethane liquids were calibrated using a bubbler with helium carrier to produce a saturated vapor. The vapor pressure was calculated to

determine the gas phase concentration of each component sent into the GC/MS. Because of this technique single point calibration was necessary.

Methanol was calibrated using the GC/MS. Pure methanol was bubbled by using helium carrier gas and the concentration in the gas phase was determined by the vapor pressure calculations. Peak curves from the GC/MS was averaged and plotted as a single point graph. Starting a point at zero was used so that we could establish a linear calibration curve from methanol readings. Similar procedure was used for formaldehyde and dimethoxymethane.

Analysis of formaldehyde gave multi components and it was not possible to find the concentration of formaldehyde. So for formaldehyde, we used methanol calibration to back calculate the formaldehyde concentration in order to establish formaldehyde calibration curve.

Concentration of dimethyl ether was varied using helium gas to establish different concentrations in gas phase. The readings were carried out directly in the GC/MS.

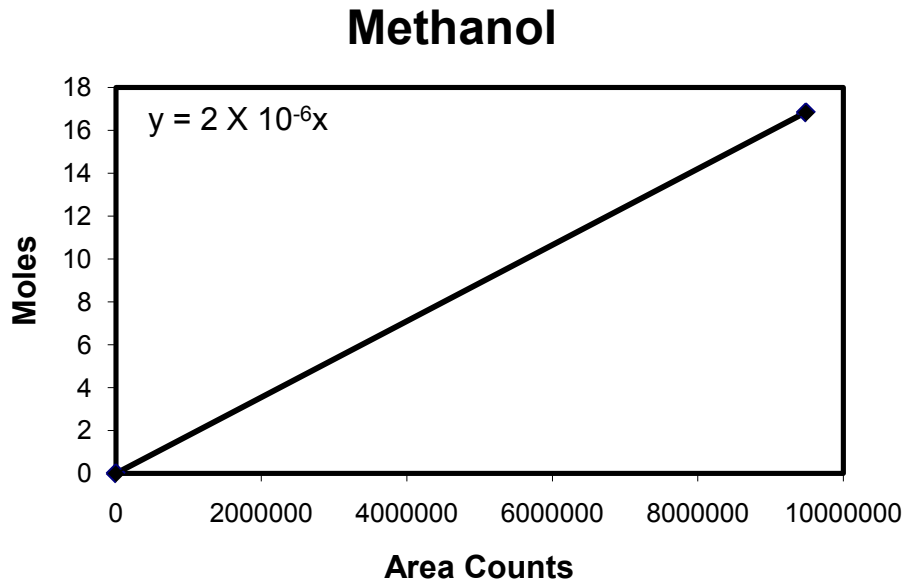


Figure (2-4): Calibration Curve for Methanol (GC/MS)

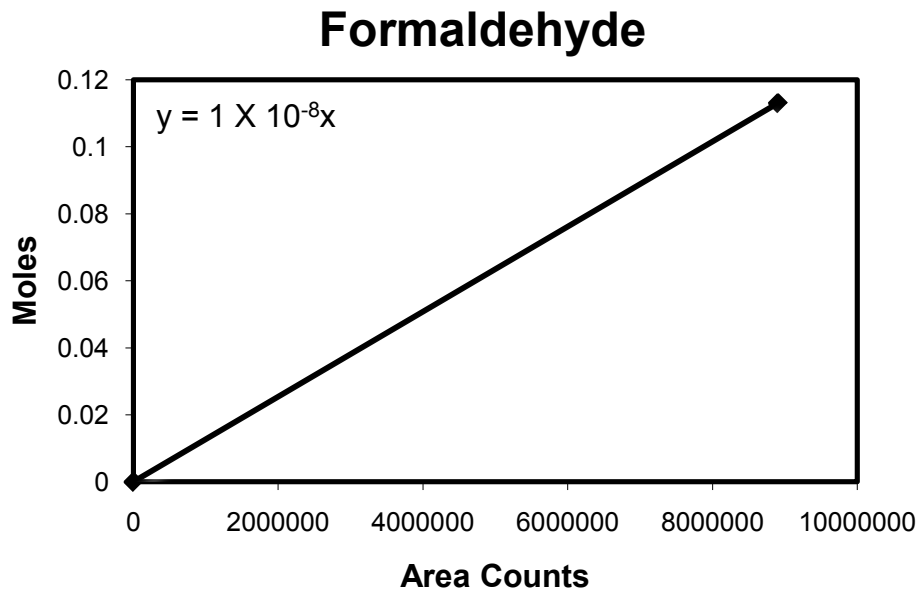


Figure (2-5): Calibration Curve for Formaldehyde (GC/MS)

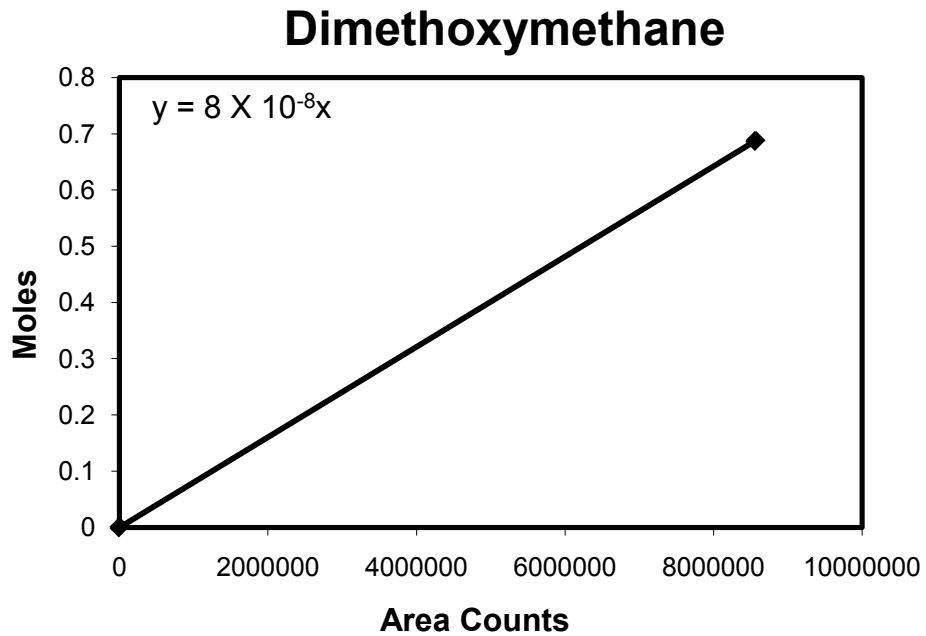


Figure (2-6): Calibration Curve for Dimethoxymethane (GC/MS)

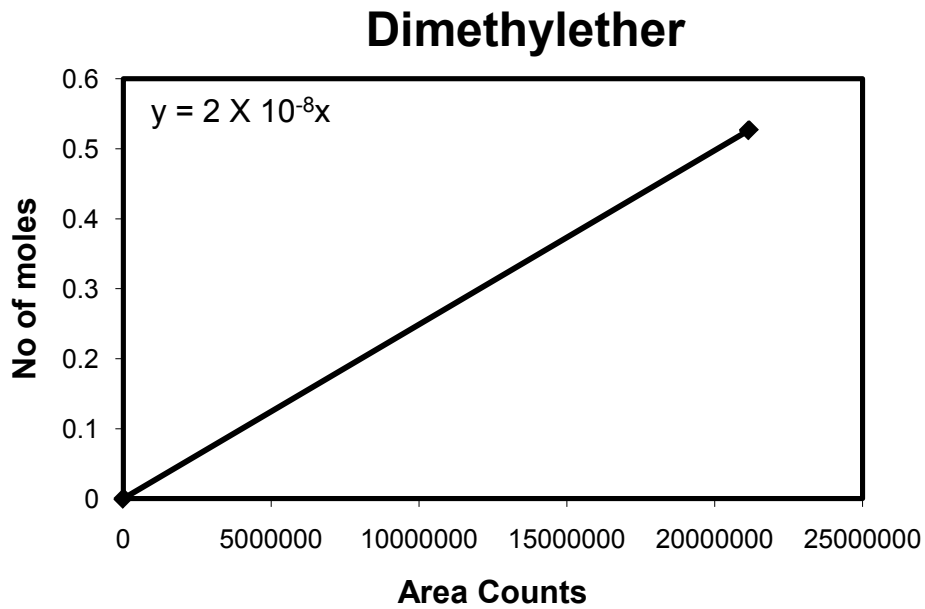


Figure (2-7): Calibration Curve for Dimethyl Ether (GC/MS)

2.6 Microcalorimetry

This work was carried out by Eric J. Dorskocil, Department of Chemical Engineering, University of Missouri.

The microcalorimetry studies was carried out in an International Thermal Instruments block in a home built system and all the catalyst samples where pretreated at 420°C under vacuum. Pure ammonia was used as the adsorbate and ammonia adsorption was carried out at room temperature.

2.7 Reaction rate calculation

The rate of each catalyst was calculated as the (concentration of methanol * flowrate of the no of moles * conversion of methanol * selectivity of each product) divided by the (weight of each catalyst taken * the surface area of each catalyst).

2.8 Selectivity calculations

The selectivity of each product was carried by using the GC/MS calibration plots from figures (2-5), (2-6) and (2-7). From the plot the number of moles of the individual product was obtained after the reaction. The selectivity (%) was calculated as the (number of moles converted to a product)/(total no of moles of all the products formed).

2.9 Surface Area Measurements

The BET surface area analysis of the catalysts under study was determined by nitrogen adsorption isotherms on a Micromeritics surface area and porosity analyzer, (Micromeritics, model ASAP 2020) using nitrogen as the carrier gas. Around 0.1 g of each sample was used for the measurement and the sample was pretreated at 420°C prior to nitrogen adsorption.

Chapter 3

Characterization of Partially Reduced Polyoxometalate Catalysts Using Ammonia Adsorption Microcalorimetry and Methanol Oxidation Studies

3.1 Introduction

Heteropolyacids (HPA's) are commonly known as strong acid catalysts both in liquid and solid forms[12]. A variety of uses for these catalysts has been discussed in a volume of chemical reviews[14]. Selective oxidation studies are extensively carried out on light hydrocarbons or alkanes like ethane, propane and butane[4], to obtain products such as acrylic acid and maleic acid since these reactants are readily available and inexpensive[1]. At present in chemical industries, the selective oxidation of hydrocarbon reactions continue to play an important role resulting in ongoing investigation of the heterogeneous catalysts that accomplish these reactions. The reason that the hetero poly acid catalysts and their salts are usually investigated for their ability to perform selective oxidation reactions is because of their structure and composition can be finely controlled. One of the major challenges is to determine the surface active sites on the metal oxides to understand the fundamental catalytic relationships for metal oxide catalysts[8]. The nature of active sites, their number and their strength on the catalyst surface determines the selectivity and conversion capabilities of the catalyst. The nature of the oxide, the charge and the radius of the metal ions will have an effect on the acidity and basicity of the catalyst[9].

Auroux and Gervasini have carried out a thermodynamic scale of surface acidity and basicity in which they determine the acid and base properties by measuring the heat of absorption and adsorption uptake of gas –phase molecules on a number of simple metal oxides[9]. The choice of the base probe molecule is important in order to aptly characterize the surface and ammonia was used because it is a small molecule and has affinity to base catalysts and most of the acid sites can be detected by ammonia[9, 10]. Bardin et al have performed acidity measurements of keggin type heteropolycompounds by a number of methods including ammonia adsorption microcalorimetry[10, 15]. Xie et al shows the use of microcalorimetry to investigate the acid site distribution on carbons[21].

Phosphomolybdic acid hydrate ($H_3PMo_{12}O_{40}$) consists of the Keggin structure which is commonly associated with heteropolyacids (HPAs) that have specific molecular architectures having metal-oxygen cluster compounds [14, 41]. The heteropolyoxomolybdates catalysts having the Keggin type structure are active for partial oxidation of alkenes and alkanes [1, 42-45]. The bifunctional nature of the heteropolyacids and their polyoxometalate as both acid and oxidation catalysts have made them effective in many different catalytic applications[1]. Especially, polyoxometalates and phosphomolybdates have been extensively investigated for the selective oxidation of light alkanes [5-7].

To study the surface metal oxide redox sites the reactivity of oxidative catalysts can be done by methanol oxidation reaction[34-38]. Previous methanol oxidation studies have been carried out on extensive number of oxides such as molybdenum oxide catalysts and vanadium oxide catalysts by Wachs and colleagues[3, 34, 40]. Methanol oxidation as referred in the review of Tatibouët[33] refers to the network of oxidation and dehydration reactions. Methanol has high reactivity towards metal oxides and has a commonality to the surface methoxy intermediate formed during the methanol oxidation and dissociative chemisorption of methanol on oxide catalysts [8]. Methanol molecules are initially adsorbed on the surface molybdenum sites as methoxy (CH_3O) species during the partial oxidation of methanol [34-39]. The products formed after the methanol oxidation are formaldehyde, methylformate, dimethoxymethane, dimethyl ether and carbon oxides. The product distribution is determined by the nature of the surface active sites [3]. The dehydration product yields the acid sites dimethyl ether, carbon oxides yield basic sites and the redox sites yield formaldehyde, methylformate and dimethoxymethane.

Work of Ueda and Suzuki showed that a molybdovanadophosphoric acid (PMo_{11}V) when treated with pyridine result is an active and selective catalyst for the conversion for propane to acrylic acid[1, 32] and later Li and Ueda showed that when pyridine is added to molybdophosphoric acid ($\text{H}_3\text{PMo}_{12}$) and heating to 420°C to activate in presence of nitrogen, improved the activity for the selective oxidation of propane to acrylic acid [1, 16]. By preheating the catalyst sample to 420°C all the organic components from the catalysts precursors or removed [14]. Niobium and pyridine-exchanged

molybdophosphoric and molybovanadophosphoric acid catalysts ($\text{NbPMo}_{12}\text{pyr}$ and $\text{NbPMo}_{11}\text{Vpyr}$) for selective oxidation of propane and butane was reported by Holles et al[1, 44].

In this paper we report how the introductions of niobium and pyridine on the parent catalyst $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ have an effect on the heat of adsorption of the catalysts as determined by ammonia adsorption microcalorimetry. In addition, the methanol oxidation reaction is used to obtain information about the acid, base and redox sites of the catalyst surface. The aim of this paper is to show how the activities of the heteropolyacid catalysts are effected when niobium and pyridine are added to them and also to better understand the acid, base and redox properties of the catalysts.

3.2 Experimental: Catalyst preparation

1) $\text{H}_3\text{PMo}_{12}\text{O}_{40}$

Phosphomolybdic acid hydrate ($\text{H}_3\text{PMo}_{12}\text{O}_{40}$) was purchased from Aldrich and used directly.

2) $\text{NbPMo}_{12}\text{O}_{40}$

Niobium exchanged phosphomolybdic acid ($\text{NbPMo}_{12}\text{O}_{40}$) catalyst was prepared by using a known method from literature[1]. Niobium pentachloride (NbCl_5) was purchased from Aldrich. The solution of Niobium pentachloride (0.3025g) and water (2.5mL) was basified with ammonium hydroxide (0.125 mL). The white precipitate formed was then

removed by filtration and the product was dissolved in an aqueous oxalic acid (0.252g in 5 mL water) to form niobium oxalate solution. The niobium oxalate solution was then added slowly to $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ (5g) dissolved in water (10 mL). The liquid was then evaporated completely by heating to 80°C and stirring the mixture continuously.

3) $\text{PMo}_{12}\text{O}_{40}\text{pyr}$

Pyridine exchanged phosphomolybdic acid ($\text{PMo}_{12}\text{O}_{40}\text{pyr}$) catalyst was prepared by first dissolving phosphomolybdic acid hydrate ($\text{H}_3\text{PMo}_{12}\text{O}_{40}$) (3g) in water and then adding an aqueous solution of pyridine (0.4205 mL in 2.5 mL water) to the solution. The liquid was then evaporated completely by heating to 80°C and stirring the mixture continuously[1].

4) $\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$

Similar procedure was used to prepare niobium and pyridine exchanged phosphomolybdic acid ($\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$) catalyst. Once niobium exchanged phosphomolybdic acid ($\text{NbPMo}_{12}\text{O}_{40}$) catalyst was prepared by the method shown above, (2g) was dissolved in water. To this solution an aqueous solution of pyridine (0.252 mL in 2.5ml water) was added. The liquid was then evaporated by heating to 80°C and stirring the mixture continuously.[1]

3.3 BET Surface Area Analysis:

The BET surface area analysis of the above catalysts was determined by nitrogen adsorption isotherms on a Micromeritics surface area and porosity analyzer,

(Micromeritics, model ASAP 2020) using nitrogen as the carrier gas. Around 0.1 g of each sample was used for the measurement and the sample was pretreated at 420°C prior to nitrogen adsorption.

3.4 Methanol Oxidation reactions:

The reactivity of supported phosphomolybdic acid derived catalysts was probed by the methanol oxidation reaction. The reactor setup consisted of a methanol bubbler, digital flow rate controller (Omega), a packed bed reactor and a GCMS (Finnegan, Trace GC ultra, Trace DSQ, Thermo Electron Corporation). The digital flow rate controller was used to control the flowrate of helium and oxygen gaseous mixture that is flowed through the methanol bubbler. The catalysts were placed in a glass tube of 6 mm and were supported by glass wool. The reactor was a downflow reactor operating at atmospheric pressure. The reactant flow was a single pass. Each catalyst sample run was pretreated to 420°C for 6 hours and held at the same temperature for 4 hours and then cooled to 260°C in 1 hour in presence of helium flow.

Feed gases consisted of helium compressed (UN 1046, 5.0 ultra high purity, (UHP)) and oxygen compressed (UN 1072). Molar feed ratio into the GCMS taken was mixture of He/O₂/MeOH at the ratio 5.6:1:1.3, the reaction was run at a standard temperature of 260°C for all the catalysts, the flowrates of helium and oxygen modified as required and the catalyst weight (0.01gm to 0.04gm) was taken to obtain around 10% methanol conversion, so that complications due to heat and mass transfer limitations can be

avoided [3]. Once feed was initiated to the reactor, the catalytic runs were taken for 2-3 hours with samples at an interval of 4 min, beginning 10 min after the methanol flow to the reactor was initiated. Product analysis was done by using the GCMS (Finnegan, Trace GC ultra, Trace DSQ, Thermo Electron Corporation) with a EquityTM-1, fused silica capillary column (30m*0.25mm*0.25 μ m film thickness). The selectivity of the products are defined in mole percentages.

3.5 Microcalorimetry:

The microcalorimetry studies was carried out in an International Thermal Instruments block in a home built system and all the catalyst samples where pretreated at 420°C under vacuum consistent with the literature[44]. Pure ammonia was used as the adsorbate and ammonia adsorption was carried out at room temperature.

3.6 Results:

The surface area measurements for the catalysts are listed in table (1). Specific surface areas were found to range from 4.6 m²/g for H₃PMo₁₂O₄₀ to 13.4 m²/g for NbPMo₁₂O₄₀Pyr. The addition of either niobium or pyridine caused an increase in surface area with the largest increase for the sample with both niobium and pyridine.

Catalyst	Surface Area (m ² /g)
H ₃ PMo ₁₂ O ₄₀	4.6
NbPMo ₁₂ O ₄₀	5.9
PMo ₁₂ O ₄₀ pyr	7.6
NbPMo ₁₂ O ₄₀ pyr	13.4

All samples, activated at 420°C

Table 1: Surface Area Measurements

Ammonia adsorption microcalorimetry results considered are shown in figure (3-1). Catalytic sites are the stronger sites on the left side in the figure (3-1) and the large number of sites on the right is physisorption sites and will not be further considered. The strong sites at less than 200 μ mol/g uptake are more closely shown in figure (3-2). The heat of adsorption for the H₃PMo₁₂O₄₀ parent catalyst is about 80 kJ/mol for initial adsorption and decreases fairly linearly to 0 kJ/mol with a total NH₃ uptake of approximately 130 μ mol/g. Incorporation of niobium, pyridine or both to the parent catalyst increases the number of adsorption sites as shown in figure (3-1). Niobium, pyridine or both increases the initial heat of adsorption by about 40 kJ/mol to 120 kJ/mol. From an initial value of 120 kJ/mol, the pyridine sample heat of adsorption decreases to ~50 kJ/mol value for physisorption (beyond 200 μ mol/g uptake). Similarly, the niobium sample decreased to approximately ~60 kJ/mol for physisorption. Finally, both niobium

and pyridine resulted in a heat of adsorption of ~80 kJ/mol for physisorption. After the initial 50 μ mol/g uptake, the catalyst with both niobium and pyridine typically had adsorption strength ~10 kJ/mol stronger than the other catalysts.

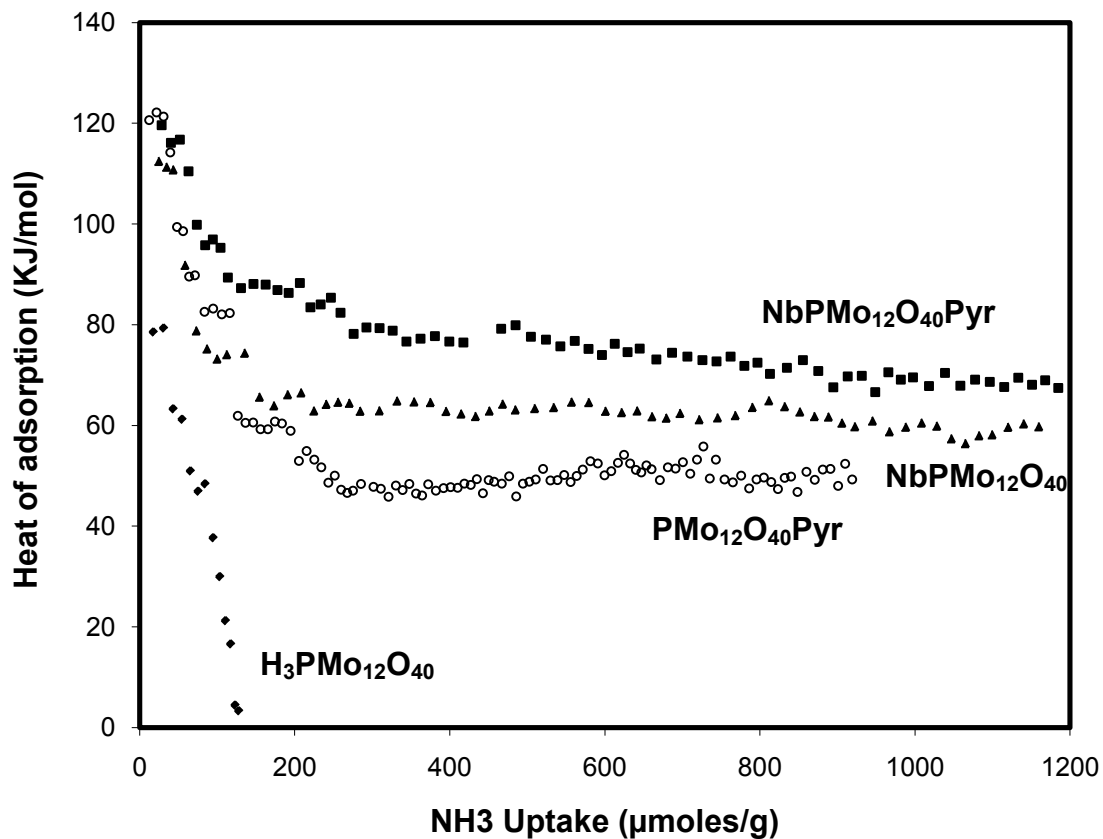


Figure (3-1) - NH₃ uptake and heat of adsorption of the catalysts showing the active sites. All the catalysts activated at 420°C

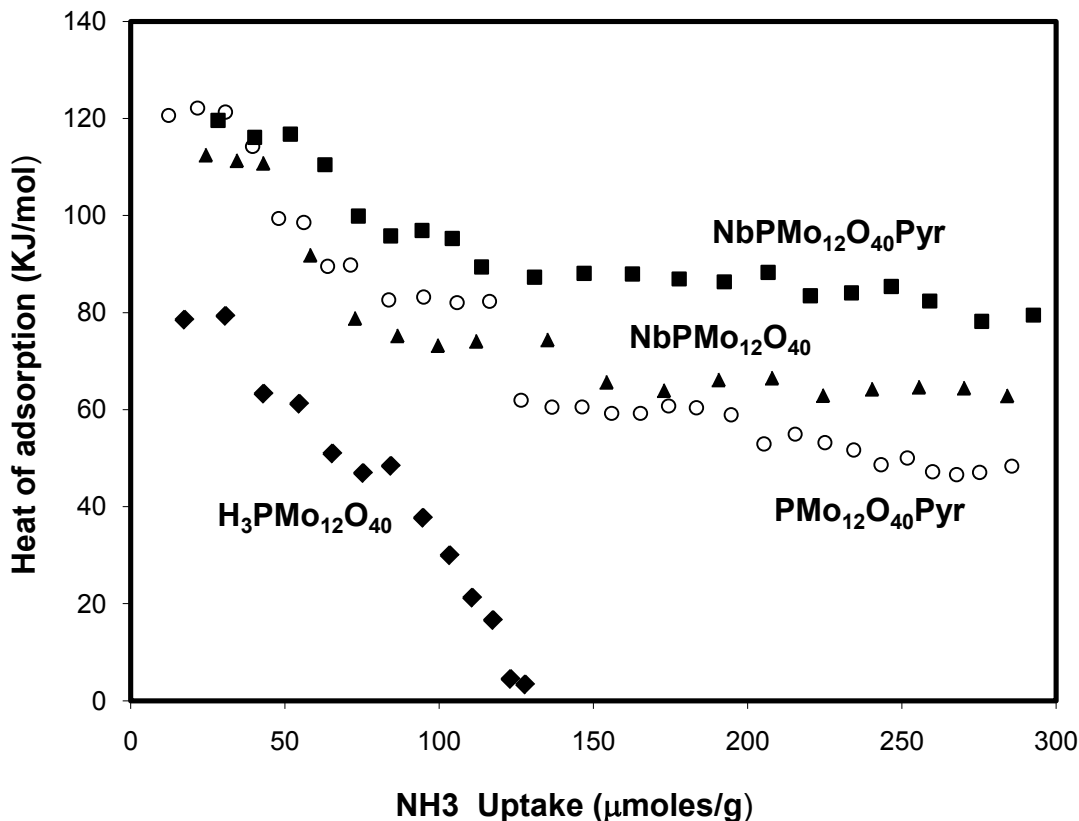


Figure (3-2) - NH₃ uptake and heat of adsorption of the catalysts showing the active sites. All the catalysts activated at 420°C

Conversion of methanol and selectivity as a function of time for H₃PMo₁₂O₄₀ catalyst are shown in figures (3-3) and (3-4). For H₃PMo₁₂O₄₀ catalyst, the conversion of methanol increased to about ~20% within 20 minutes and then decreased. At approximately 50 minutes time on stream, the conversion was 10% and the selectivity at this point was used for comparison with the other catalysts. The products formed from the reaction are dimethyl-ether (DME) from acidic sites and dimethoxy-methane (DMM) from redox sites. The selectivity of the redox product DMM was as high as 95% and that of the

acidic product DME 5% at 10% conversion of methanol. Selectivity as a function of time is shown in figure (3-4). Although conversion decreased after an initial incubation period, selectivity was fairly constant over the entire time.

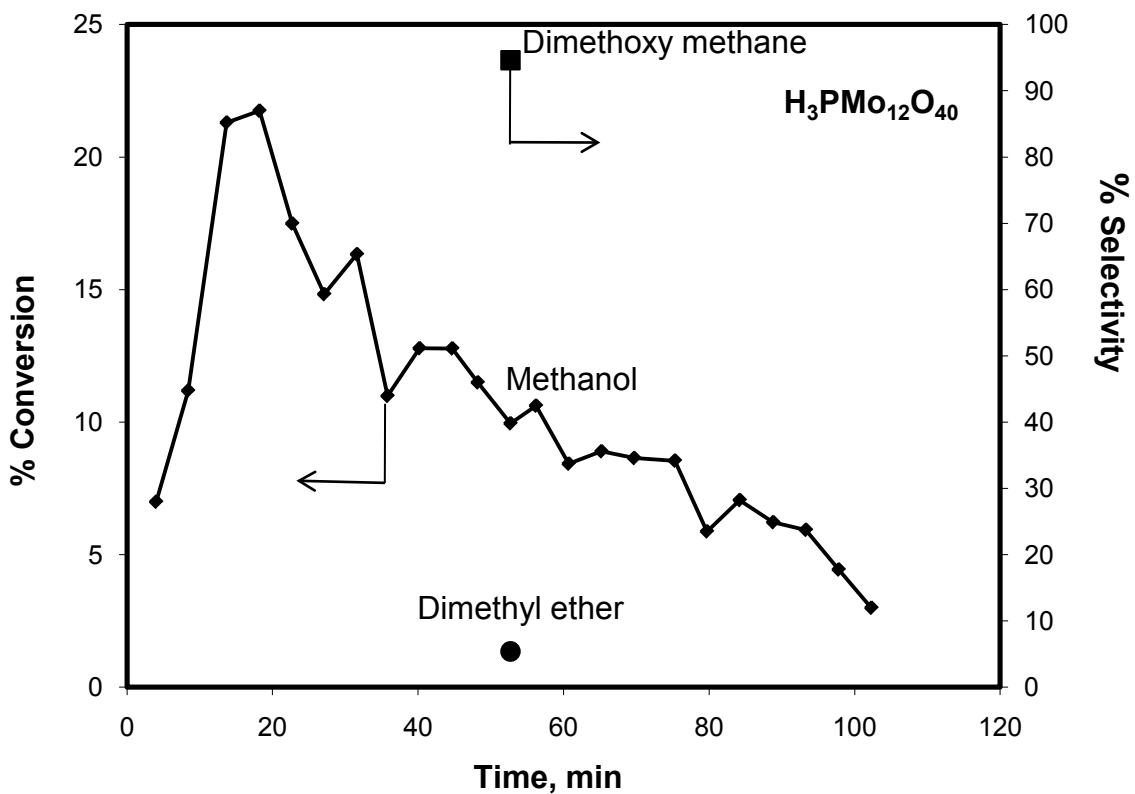


Figure (3-3) - Conversion and selectivity of $H_3PMo_{12}O_{40}$ catalyst as a function of time. The reaction was carried out at $260^\circ C$ and with 0.02g of catalyst and a total flowrate of 96.2 (ml/min) (He/O₂/MeOH = 67.69/11.95/16.2 ml/min)

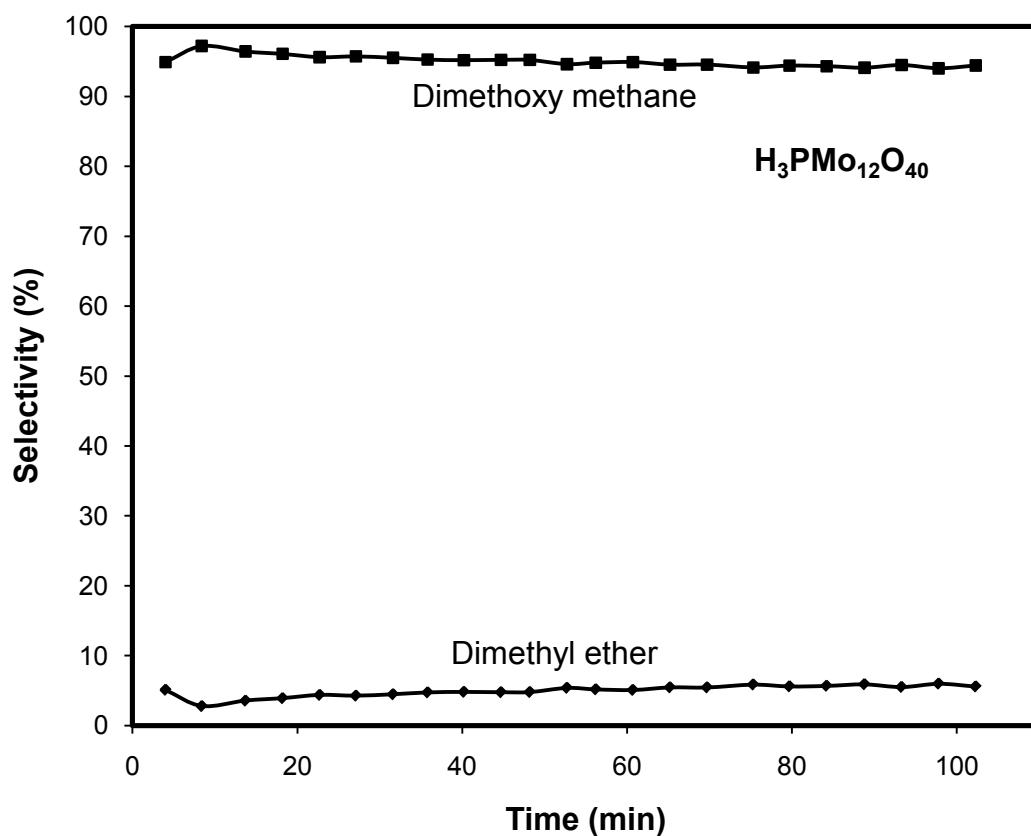


Figure (3-4) - Selectivity of all products as a function of time of $H_3PMo_{12}O_{40}$ catalyst. The reaction was carried out at $260^\circ C$ and with 0.02g of catalyst and a total flowrate of 96.2 (ml/min) ($He/O_2/MeOH = 67.69/11.95/16.2$ ml/min)

The conversion of methanol and selectivity as a function of time for $NbPMo_{12}O_{40}$ catalyst are shown in figure (3-5) and (3-6). Here the conversion of methanol was maintained at a range of about 10-15% for almost 120 minutes and did not decrease over time like the $H_3PMo_{12}O_{40}$ catalyst. The products after reaction are DME (acidic) and DMM (redox). The selectivity of the redox product DMM was slightly lower compared to $H_3PMo_{12}O_{40}$

catalyst at 93% with a corresponding slight increase in the selectivity of DME (acidic) product to 7%.

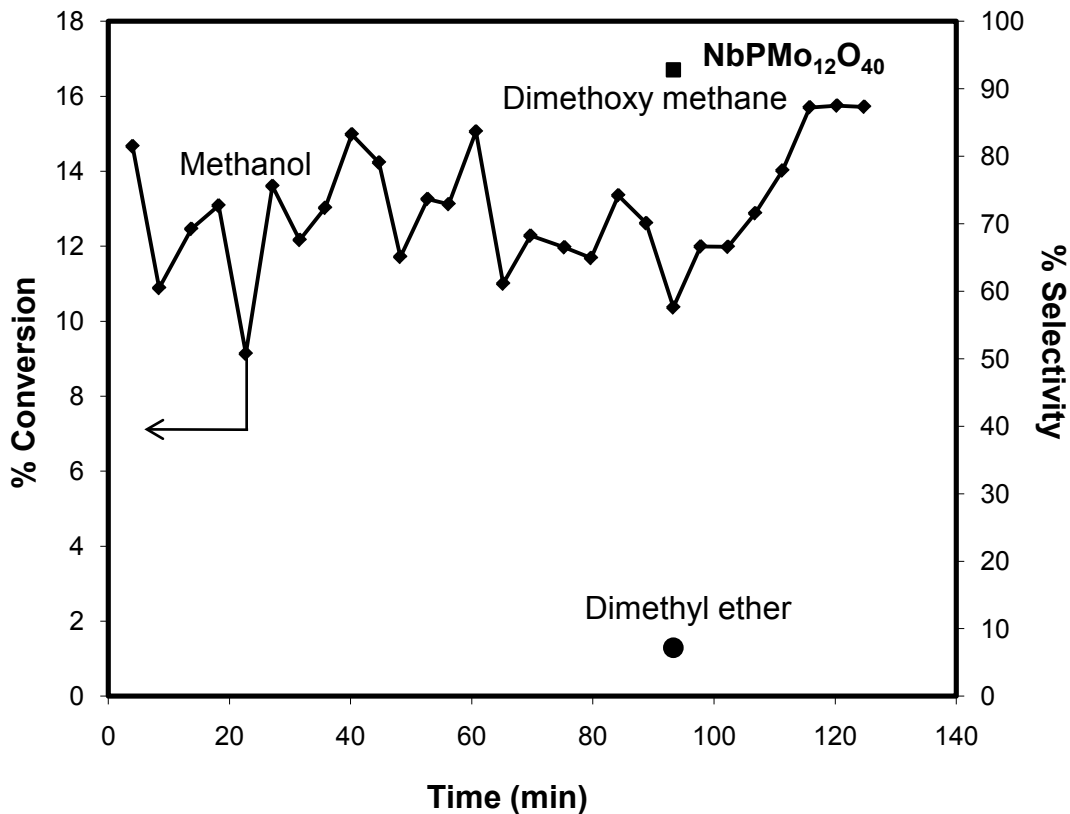


Figure (3-5) - Conversion and selectivity of NbPMo₁₂O₄₀ catalyst as a function of time. The reaction was carried out at 260°C and with 0.04g of catalyst and a total flowrate of 108.2 (ml/min) (He/O₂/MeOH =76.5/13.5/18.2 ml/min).

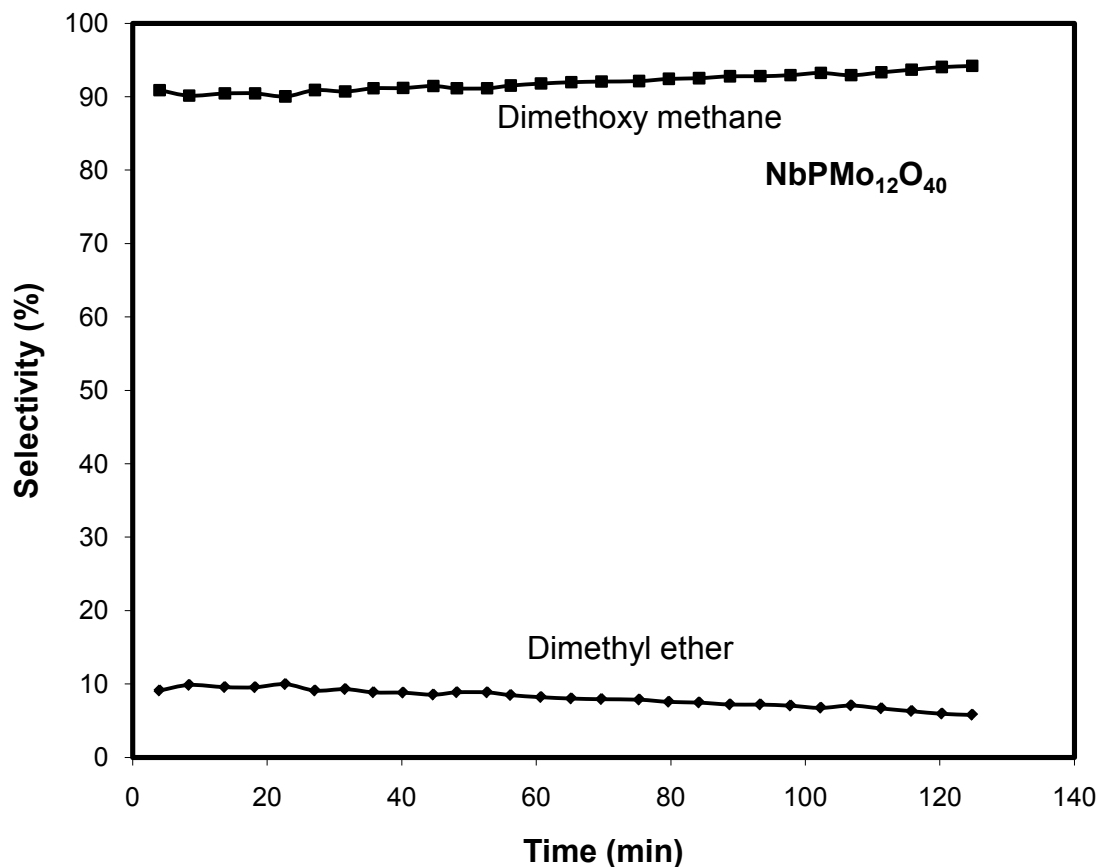


Figure (3-6) - Selectivity of all products as a function of time of $\text{NbPMo}_{12}\text{O}_{40}$ catalyst. The reaction was carried out at 260°C and with 0.04g of catalyst and a total flowrate of 108.2 (ml/min) ($\text{He}/\text{O}_2/\text{MeOH} = 76.5/13.5/18.2$ ml/min).

The conversion of methanol and selectivity as a function of time for $\text{PMo}_{12}\text{O}_{40}\text{pyr}$ catalyst are shown in figure (3-7) and (3-8). The conversion of methanol was maintained at around 10% for about 75 minutes and then started to decrease with time. The products formed are DME (acidic), DMM (redox) and a very small amount of formaldehyde (redox). At 10% conversion, the selectivity of the acidic product DME was 62%, the

selectivity of the redox product DMM was 38 % and a small selectivity of formaldehyde <1.0% was observed. With pyridine in the catalyst the selectivity of the acidic product increased and the selectivity of the redox product decreased, in contrast with the parent and niobium exchanged catalyst. In figure (3-8), the selectivity of all products as a function of time is shown for $\text{PMo}_{12}\text{O}_{40}\text{pyr}$ catalyst. Here it is seen that the selectivity of DME (acidic) is higher initially at around 75% and then decreases to about 45% over 150 minutes. The selectivity of DMM (redox) was initially low at about 23% and then increased to around 60% over 150 minutes. After about 80 minutes the selectivity of DMM (redox) overtakes the selectivity of DME (acidic). Following an initial transient, the selectivity of DME decreased and the selectivity of DMM increased with time on stream. These selectivity changes occur simultaneously with the catalyst deactivation. In contrast with the other catalysts, only selectivity for the pyridine sample showed the most variability as a function of time on stream.

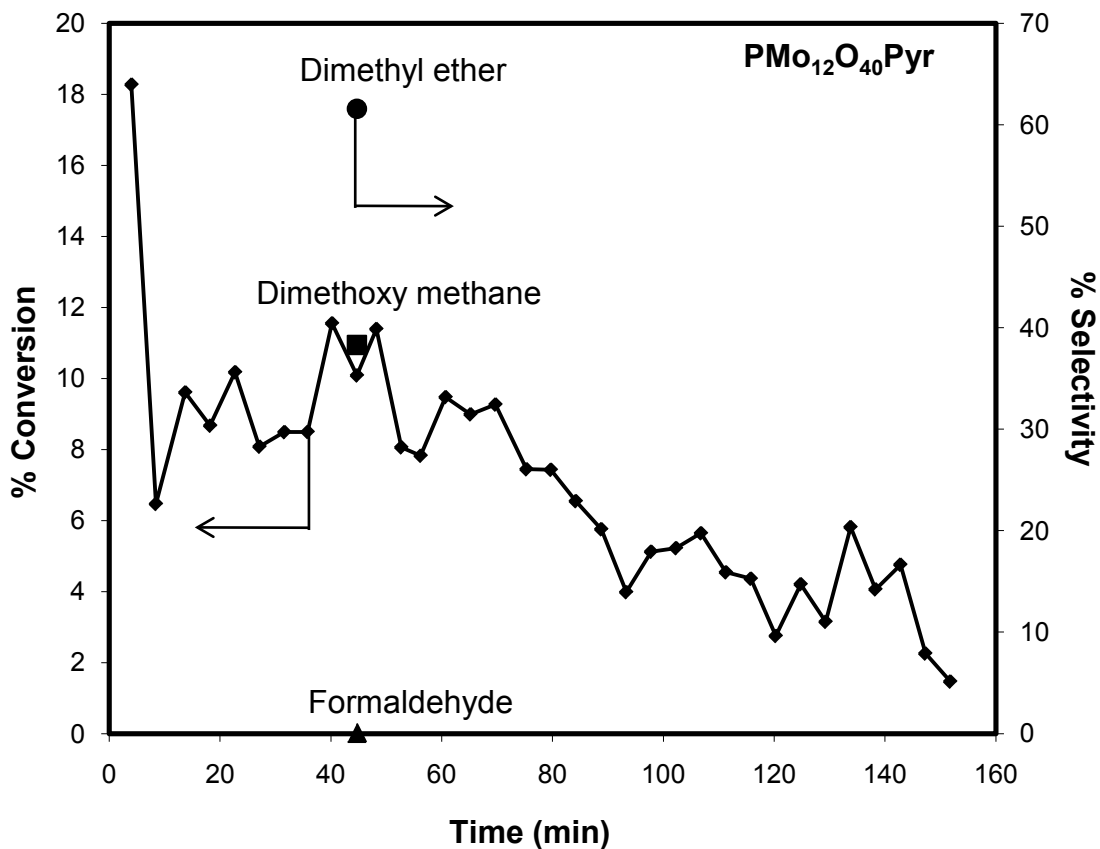


Figure (3-7) - Conversion and selectivity of $\text{PMo}_{12}\text{O}_{40}\text{Pyr}$ catalyst as a function of time. The reaction was carried out at 260°C and with 0.04g of catalyst and a total flowrate of 108.2 (ml/min) ($\text{He}/\text{O}_2/\text{MeOH} = 76.5/13.5/18.2$ ml/min).

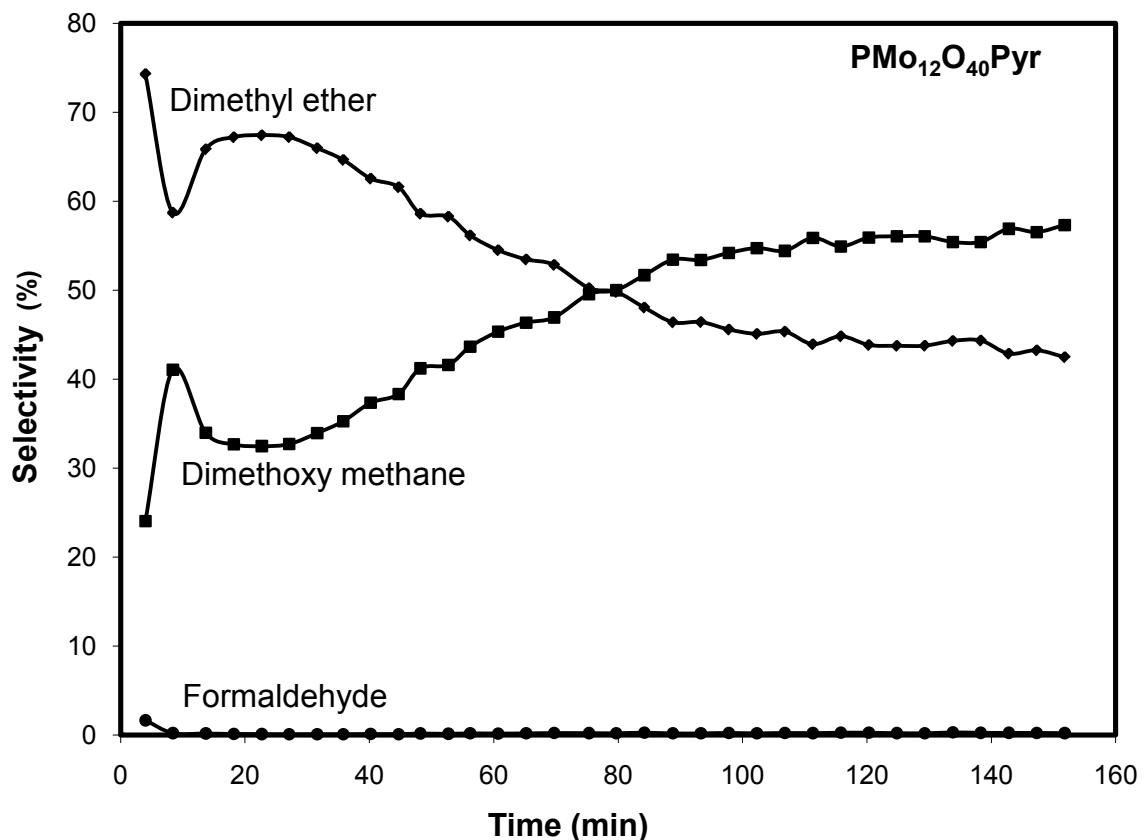


Figure (3-8) - Selectivity of all products as a function of time of $\text{PMo}_{12}\text{O}_{40}\text{Pyr}$ catalyst. The reaction was carried out at 260°C and with 0.04g of catalyst and a total flowrate of 108.2 (ml/min) ($\text{He}/\text{O}_2/\text{MeOH} = 76.5/13.5/18.2$ ml/min).

The conversion of methanol and selectivity as a function of time for $\text{NbPMo}_{12}\text{O}_{40}\text{Pyr}$ catalyst are shown in figure (3-9) and (3-10). The conversion of methanol was around 10% between 20-58 minutes and increased gradually with time. The products formed are DME (acidic), DMM (redox) and very small amount formaldehyde (redox). The

selectivity of the acidic product DME was very high at 95%, the selectivity of the redox product DMM was 5% and a small selectivity to formaldehyde of < 1% was seen.

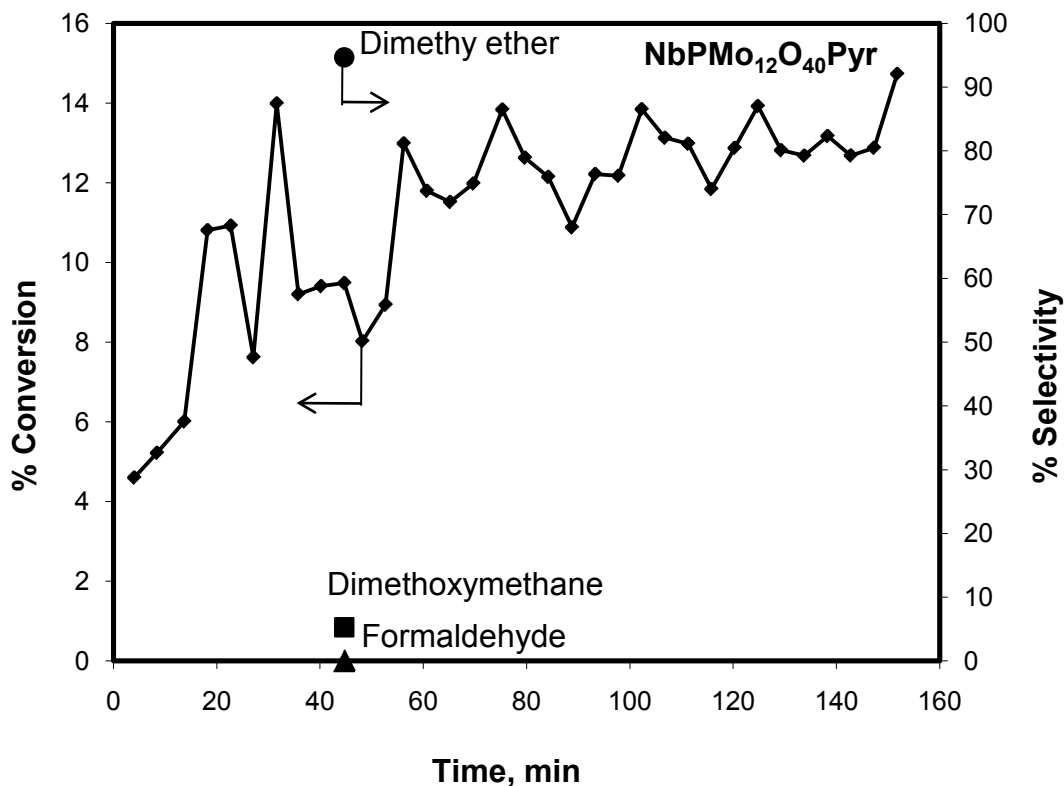


Figure (3-9) - Conversion and selectivity of NbPMo₁₂O₄₀Pyr catalyst as a function of time. The reaction was carried out at 260°C and with 0.01g of catalyst and a total flow-rate of 157.3 (ml/min) (He/O₂/MeOH =115.2/20.44/27.34 ml/min).

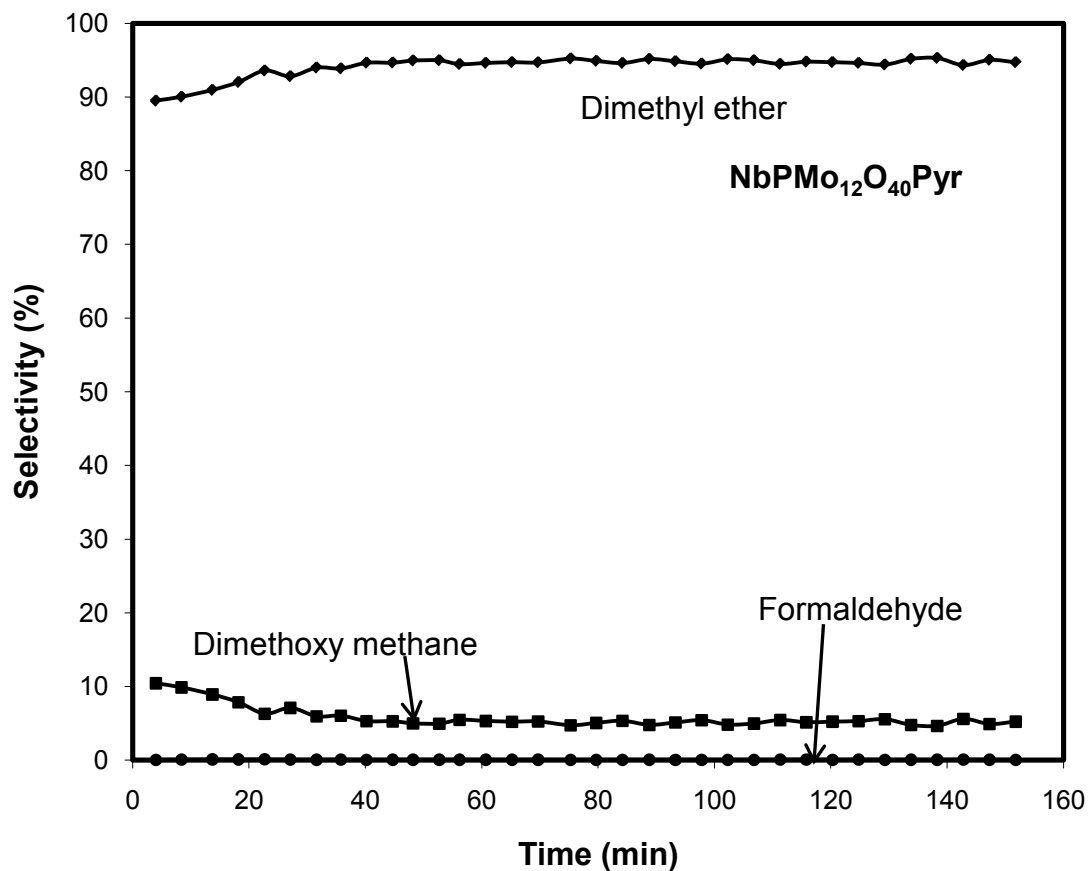


Figure (3-10) - Selectivity of all products as a function of time of NbPMo₁₂O₄₀Pyr catalyst. The reaction was carried out at 260°C and with 0.01g of catalyst and a total flow-rate of 157.3 (ml/min) (He/O₂/MeOH =115.2/20.44/27.34 ml/min).

The selectivity of all products as a function of time is shown in figure (3-10) for NbPMo₁₂O₄₀pyr catalyst. When niobium and pyridine was combined with the parent catalyst the selectivity of DME (acidic) product was high, above 90%, and did not decrease as in the case of PMo₁₂O₄₀pyr catalyst figure (3-8). The selectivity of DMM (redox) decreased slightly from about 10 % and remained constant around 6%. Small

traces of formaldehyde (redox) were also noticed. In contrast with the pyridine only sample, all selectivities were fairly constant as a function of time.

In table (2) the rate of reactivity of the products for each catalyst is reported at 10 % conversion. When niobium was incorporated, the rate of formation both acidic and redox products decreased when compared to the parent catalyst.. Addition of pyridine to the parent catalyst decreased the rate of DMM (redox) production by a factor of 6 and increased the production rate of the acidic product by a factor of 4 compared to the parent catalyst. The highest reaction rate to the acidic product occurs when both niobium and pyridine was incorporated to $H_3PMo_{12}O_{40}$ catalyst. This rate was 7.5 times the rate of the next highest catalyst.

Catalyst	DME(Acidic) (mmol/min m^2)	DMM(Redox) (mmol/min m^2)	Formaldehyde(Redox) (mmol/min m^2)
$H_3PMo_{12}O_{40}$	1.5×10^{-7}	2.7×10^{-6}	-
NbPMo ₁₂ O ₄₀	1.0×10^{-7}	1.3×10^{-6}	-
PMo ₁₂ O ₄₀ pyr	6.9×10^{-7}	4.2×10^{-7}	9.7×10^{-10}
NbPMo ₁₂ O ₄₀ pyr	5.1×10^{-6}	2.8×10^{-7}	3.2×10^{-9}

Table 2: Reactivity of the catalyst (mmol/min m^2) at 260°C, around 10% conversion.

Catalyst reactivity of the products formed using methanol as substrate

In table (3) the selectivity of the products at 10 % conversion is reported. The parent catalyst had selectivity >90% for DMM (redox). With the addition of niobium to $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ catalyst a slight increase of about ~2% was noticed in the selectivity of the DME (acidic). With the pyridine exchanged catalyst, the selectivity of DME increased to about ~62%, selectivity of DMM (redox) decreased to about ~38% and for formaldehyde (redox) it was > 1% at 10% conversion. The niobium and pyridine exchanged catalyst had selectivity to DME (acidic) at ~95%, almost completely reversing the high selectivity of the parent catalyst from DMM (redox) to DME (acidic). The selectivity of formaldehyde was >1%.

Catalyst	DME(Acidic)	DMM(Redox)	Formaldehyde(Redox)
$\text{H}_3\text{PMo}_{12}\text{O}_{40}$	5.4	94.6	-
$\text{NbPMo}_{12}\text{O}_{40}$	7.2	92.8	-
$\text{PMo}_{12}\text{O}_{40}\text{pyr}$	61.5	38.3	0.087
$\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$	94.6	5.3	0.059

Table 3: Catalyst Selectivity (%) at 260°C, around 10% conversion.

Catalyst selectivity of the products formed using methanol as substrate

3.7 Discussion:

The literature reactivity results for production of maleic acid from n-butane show that the most active and selective catalyst is the niobium and pyridine exchanged phosphomolybdic acid ($\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$)[1]. However, by closely examining the activity and selectivity effect for each component, a better understanding of the contribution of each component to the catalyst can be elucidated. The parent $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ catalyst showed the lowest activity with selectivity mainly to combustion products[1]. The addition of niobium to the parent catalyst resulted in increased activity with the selectivity now mainly to the desired maleic acid product[1]. The addition of pyridine to the parent catalyst also resulted in increased activity and selectivity to the desired product. Pyridine increased the activity more than niobium, but both had similar selectivities. Finally, the combination of both niobium and pyridine resulted in the highest activity and selectivity.

Auroux and Gervasini have reported the study of acidity and basicity on metal oxides surfaces[9] and have used microcalorimetry in order to determine the number and character of basic and acidic surface sites. Adsorption microcalorimetry has also been used to study the acidity of heteropolycomponents using ammonia[10, 15, 21, 22]. Interactions with acid sites in solids are often studied with ammonia because it is one of the simplest molecules and is also the most studied basic probe molecule[15]. Strong acids bind more strongly with ammonia than weaker acids.

When pyridine was added to the parent catalyst, the initial heat of adsorption was ~10 kJ/mol higher than for niobium addition to the parent catalyst. At increased uptake, the pyridine sample heat of adsorption was equal to or slightly greater than the niobium sample until the ammonia dosing exceeded 120 $\mu\text{mol/g}$. When both niobium and pyridine were incorporated in the parent sample, the initial heat of adsorption was equivalent to the pyridine only sample. However, as ammonia dosing increased, the niobium and pyridine sample continued to show stronger sites than either of the samples with only niobium or pyridine. Thus, the combination of both niobium and pyridine resulted in a higher number of stronger sites. These sites were 10 – 20 kJ/mol stronger after the initial adsorption. While the most active catalyst for selective oxidation of n-butane ($\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$) did have a large number of stronger acid sites, there are no significant differences between the catalysts, which might account for the dramatic increase in activity reported in the literature[1].

The ammonia adsorption result for $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ obtained by Jozefowicz et al demonstrated an initial heat of 150 kJ/mol when treated at 323 K. Bardin et al showed that the sample pretreated at 473K had a higher heat of adsorption ~120 kJ/mol than when treated at 573 K, which was ~100 kJ/mol[10]. The decreasing heat of adsorption as pretreatment temperature increased likely results because the structure started to decompose as the pretreatment temperature increased [10]. The site density also decreased from about 1050 $\mu\text{mol/g}$ to as low as 200 $\mu\text{mol/g}$ as the pretreatment temperature increased from 473 K to 573 K [10]. The results in this paper in figure (3-1) and (3-2) shows that the parent catalyst $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ which was pretreated at a higher

temperature of 698 K had a lower heat of adsorption of about ~80 kJ/mol. The total uptake also decreased to 130 $\mu\text{moles/g}$. This loss of adsorption strength and sites is consistent with the decomposition of the keggin structure as pretreatment temperature increases as shown by phosphorous NMR[45]. However, when niobium, pyridine or both was incorporated into the parent $\text{H}_3\text{PMO}_{12}\text{O}_{40}$ catalyst that was pretreated at 698 K, the initial heat of adsorption is the same as with that of the parent catalyst pretreated at 473K shown in the work of Bardin et al [10]. The number of strong adsorption sites is also increased upon incorporation of niobium, pyridine or both.

Previously, Xue et al have shown that the ammonia adsorption studies on MoO_3 at 423K produced initial heat lower than 20kJ/mol [31]. Thus, the active sites in these catalysts are clearly not just molybdenum oxide. Jin et al have reported that the initial heat of adsorption to be about ~90 kJ/mol for Nb_2O_5 ammonia adsorption studies[28]. Sun et al have showed at 423 K the initial heat of adsorption for Nb_2O_5 was ~150 kJ/mol with ammonia uptake of 280 $\mu\text{mol/g}$ [29]. But, Petre et al have shown the initial heat of adsorption to be ~125 kJ/mol at 353 K and 423 K with ammonia uptake of 190 $\mu\text{mol/g}$ and 250 $\mu\text{mol/g}$ respectively for Nb_2O_5 . While these initial heats for ammonia adsorption on Nb_2O_5 are consistent the values for on niobium containing catalyst, we also observe similar heats for non-niobium containing catalysts (i.e., pyridine only).

During oxidation of methanol, the surface methoxy groups are the intermediate species in the production of partially oxygenated reaction products such as formaldehyde, dimethyl ether, dimethoxymethane, methylformate etc.[33, 46]. The products formed depend on

the nature of the active sites: acidic, basic or redox. The products obtained from the reaction of our catalysts are dimethyl ether (acidic), dimethoxymethane (redox) and formaldehyde (redox). From Tatibouët [33], the methanol reaction on oxide surfaces is very sensitive to the nature of surface active sites which can lead to the formation of various products by methanol oxidation. Methanol oxidation reactions can be categorized into oxidation reactions that need oxygen and dehydration reactions that need no oxygen. The formation of all products except for DME (acidic) needs at least one oxidation step. Selectivity of DME (acidic) is attributed to the dehydration capability of the catalyst which in turn is related to its own acidic character [8].

Methanol oxidation reaction result from figure (3-3) for $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ catalyst shows conversion of methanol and selectivity at 10% conversion as a function of time. After the initiation period, the catalyst activity decreases over time and has high selectivity for the redox product DMM ~95 % and about ~5 % for the acid product DME. The selectivity of the products as a function of time from figure (3-4) shows that there is no change in the selectivity even though the catalyst deactivates as shown in figure (3-3). Although no direct literature comparisons are available, this catalyst is known to decompose at pretreatment conditions in excess of 440°C to MoO_3 [45]. Wachs et al reported high selectivity of redox products for methanol oxidation studies on MoO_3 [3, 8]. The presence of similar selectivity from $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ and MoO_3 suggests the similarity of active sites.

The addition of niobium to the parent catalyst stabilizes the catalyst as shown in figure (3-5). The conversion is almost stable and the catalyst does not deactivate as that of $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ in figure (3-5). With the addition of niobium, the selectivity of the acid product increased slightly to about ~7% and the selectivity of DMM (redox) decreased slightly to about ~93%. Similar to $\text{H}_3\text{PMo}_{12}\text{O}_{40}$, the selectivity for the $\text{NbPMo}_{12}\text{O}_{40}$ catalyst remained constant as a function of time on stream. In contrast with MoO_3 , methanol oxidation studies carried out by Wachs et al on Nb_2O_5 demonstrated a high selectivity for the acidic product [8, 47]. Thus, the slight increase in selectivity of the acid product when niobium was added to the parent catalyst is consistent with the addition of some active niobium sites.

In figure (3-7) when pyridine is added to the parent catalyst $\text{H}_3\text{PMo}_{12}\text{O}_{40}$, it is seen that after 60 minutes the catalyst starts to deactivate. However, the important observation was the increase in the selectivity of the acid product which was as high as ~62% compared with that of $\text{NbPMo}_{12}\text{O}_{40}$ which was less than 10% for acidic product. The selectivity of the redox product dropped to ~38% (at 10 % conversion) from about ~92% with the addition of pyridine instead of niobium to the parent catalyst. Small traces of formaldehyde were also observed (<1%). Figure (3-8) shows the selectivity of the products as a function of time and the important finding was the selectivity of DME (acidic) was high at about ~75 % and later decreased to about 45 % over time and the selectivity of the redox product increased gradually from about ~23 % to about ~60 %. The switch in product selectivity occurred in parallel with the loss of activity. The selectivity of the redox product was more than that of acid product after about 80

minutes. This result is consistent with the ammonia adsorption results in figure (3-1) where it is seen that the catalyst with pyridine has the highest initial heat of adsorption and is thus the strongest acid. Pyridine increases the strength of acid sites in the catalyst but does not stabilize the catalyst like niobium (figure (3-5) and (6)).

When both niobium and pyridine are incorporated into the parent catalyst $\text{H}_3\text{PMo}_{12}\text{O}_{40}$, the methanol oxidation result for the conversion and selectivity of the products as a function of time are shown in figure (3-9) and (3-10). The conversion of the catalyst remains constant over time (figure (3-9)) which is similar to the $\text{NbPMo}_{12}\text{O}_{40}$ catalyst (figure (3-5)). The selectivity of the acid product, dimethyl ether, is very high at ~95% and that of the redox product, dimethoxy methane, was about ~5% at 10% conversion of methanol. This selectivity shows similarity with $\text{H}_3\text{PMo}_{12}\text{O}_{40}\text{pyr}$ catalyst where the selectivity of DME (acidic) was high initially.

From the figure (3-10) it can be observed that after a very small initial increase, the selectivity of the acid product remained constant. A corresponding small initial decrease was observed in the selectivity of the redox product and it then remained constant. These results agree fairly well with that of the ammonia adsorption microcalorimetry study in figure (3-1) and (3-2), where the $\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$ catalyst has consistently stronger acid sites than the other catalysts. The presence of niobium along with pyridine is necessary to obtain the maximum activation of the catalyst. Studies done on molybdenum-based pyridine exchanged heteropolyanion catalysts by Holles et al showed that the presence of

niobium increased the activity and productivity significantly for n-butane oxidation to maleic acid[4, 14, 15].

In this study, the rate of acid, base and redox sites at 260°C for conversion of methanol around 10% shows that the addition of pyridine and niobium has important effects on the parent catalyst. We did not detect the presence of any base sites in the product stream; either they were non-existent or too small to measure. Wachs et al observed redox and acidic products for methanol oxidation of MoO₃ at 300°C and the ratio was 6:1 [8]. Our results also show redox and acidic products for H₃PMo₁₂O₄₀ catalyst and the selectivity of redox products was high. The ratio of redox to acidic product selectivity at 10% conversion at 260°C was 19: 1 for the parent catalyst H₃PMo₁₂O₄₀. Wachs et al reported only acidic and no redox and base product for Nb₂O₅ during methanol oxidation at 300°C [8]. While our results show both redox and acidic products for the catalyst with niobium, it should be noted that NbPMo₁₂O₄₀ catalyst is still mostly Mo with a small amount of niobium. As expected from the literature, the presence of niobium did slightly increase the selectivity of the catalyst to the acidic product.

From Wachs et al work, niobium oxide results only in the acidic product [8]. The addition of niobium decreased the ratio of redox and acidic product selectivity to 13:1, clearly showing slightly higher selectivity of the acidic product. The slight increase in selectivity for the NbPMo₁₂O₄₀ catalyst agrees with the results shown by Wachs et al, where only acidic product was found for Nb₂O₅. With the pyridine exchanged catalyst the ratio of redox to acidic product was 1:1.6 at 10% conversion and inverted compared to

the parent and niobium exchanged catalyst. This clearly shows that pyridine has a major impact on the acidic product selectivity. From the work of Wachs, no previous oxide gave more acid than redox products[8]. Finally, when both niobium and pyridine was incorporated into the parent catalyst, the ratio of the selectivity of the redox and acidic product further decreased to 1:19. This ratio is the opposite of the parent catalyst and higher than the pyridine only catalyst.

Wachs et al has reported three oxides that favor redox product over acidic product: V_2O_5 , MoO_3 and Fe_2O_3 [8]. The oxides that only favor acidic product (no redox/base) reported by them are Nb_2O_5 , P_2O_5 , Ga_2O_3 , WO_3 , Ta_2O_5 and Al_2O_3 [8]. But, none of the oxides reported have the same ratio of redox to acidic product that has been observed in our study for the niobium and pyridine exchanged catalyst. Only two oxides TiO_2 and SiO_2 have presence of acidic and base product in them[8].

From these results it can be observed that niobium, when added to the parent catalyst, stabilizes the sites and keeps the catalyst active. The pyridine and niobium exchanged catalyst has the most activity and selectivity for acid sites. These results are on similar grounds as that of the results found in the n-butane reactivity studies carried out by Holles et al[1].

From the results of ammonia adsorption and methanol oxidation of the heteropolyacid catalysts in our study, it can be noted that the pyridine is main driving factor that increases the strength of active sites. The rate of the reaction for the acidic product is

higher than that of the redox for catalyst $\text{PMo}_{12}\text{O}_{40}\text{pyr}$ and the catalyst $\text{NbPMo}_{12}\text{O}_{40}\text{pyr}$ (Table 2, at 10 % conversion). This is well reflected with their selectivity in this work (Table 3). In the results of the paper by Holles et al it was shown that niobium and pyridine-exchanged salts of molybophosphoric acid had more activity and selectivity for the selective oxidation of butane[1]. Pyridine increases the surface area of the catalyst so does niobium. But with niobium though the acid sites are increased, it is the redox sites that are very active. Pyridine being more acidic increases the acid sites on the catalyst surface and has been shown in the results of ammonia adsorption (figure (3-1) and (3-2)).

3.8 Conclusion:

Microcalorimetry and methanol oxidation studies on polyoxometalate catalysts have been performed. The addition of either niobium or pyridine to the parent $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ catalyst results in increased site strength but both have similar heats of adsorption. When both niobium and pyridine are present in the catalyst it does not result in higher ammonia heat of adsorption. However, more strong sites are present when the catalyst is exchanged with both niobium and pyridine.

During methanol oxidation, the parent catalyst $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ and the one with niobium only demonstrated high selectivity for the redox product. The parent catalyst has high activity for redox product which has been shown with its selectivity. But with niobium exchanged catalyst, even though it has high selectivity for redox product, there is a slight increase in the selectivity of the acidic product. The addition of pyridine increases the selectivity for acidic product but is not well reflected with its activity. The catalyst

exchanged with both niobium and pyridine has high activity for acidic products than redox and the selectivity is also very high for acidic product.

Chapter 4

Conclusions

Microcalorimetry and methanol oxidation studies on polyoxometalate catalysts have been performed. The addition of either niobium or pyridine to the parent $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ catalyst results in increased site strength but both have similar heats of adsorption. When both niobium and pyridine are present in the catalyst it does not result in higher ammonia heat of adsorption. However, more strong sites are present when the catalyst is exchanged with both niobium and pyridine.

During methanol oxidation, the parent catalyst $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ and the one with niobium only demonstrated high selectivity for the redox product. The parent catalyst has high activity for redox product which has been shown with its selectivity. But with niobium exchanged catalyst, even though it has high selectivity for redox product, there is a slight increase in the selectivity of the acidic product. The addition of pyridine increases the selectivity for acidic product but is not well reflected with its activity. The catalyst exchanged with both niobium and pyridine has high activity for acidic products than redox and the selectivity is also very high for acidic product.

4.1 Recommendations for Future Works

This research work focused on determining the acid, base and redox contribution of niobium and pyridine components of heteropolyacid based selective oxidation catalyst. This family of catalysts has been shown to successfully convert butane to maleic acid. While these catalysts can also be used to convert propane to acrylic acid, the presence of

additional vanadium is important. Previously, in catalyst reactivity studies using propane as a substrate, the presence of vanadium in the niobium and pyridine exchanged catalyst lead to 50% selectivity of acrylic acid, but without vanadium the selectivity dropped to 6% for acrylic.

Since vanadium appears essential for high selectivity to acrylic acid, it is clearly providing a separate contribution to the catalyst. It will be interesting to see the effect of the ratio of niobium/pyridine/vanadium in these catalysts, and to know what will be minimum niobium required to stabilize the catalyst. The amount of niobium, pyridine and vanadium can be altered to optimize the catalyst activity. Similar to the studies discussed in this thesis, it is unknown if vanadium contributes to the acid, base or redox component of the catalyst. Thus, performance of ammonia adsorption microcalorimetry and methanol oxidation studies on these catalysts with vanadium could provide evidence for the role of vanadium in the selective oxidation of propane to acrylic acid.

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